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(54) Title: PROCESS FOR IMPROVING FLOW CHARACTERISTICS OF CRYSTALLINE IBUPROFEN



(57) Abstract

A process for producing crystalline ibuprofen having a crystal habit characterized by a particle length larger than 75 microns average and a length to width aspect ratio of greater than about 4 to 1 to about 5 to 1. The process involves crystallizing ibuprofen from a saturated solution of ibuprofen in a liquid hydrocarbon solvent by seeding and cooling such solution to a temperature of about 0 °C to about -20 °C at a rate to retard primary nucleation and promote secondary nucleation. The crystalline ibuprofen is separated from the slurry produced from such cooling.

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**PROCESS FOR IMPROVING
FLOW CHARACTERISTICS OF CRYSTALLINE IBUPROFEN**

FIELD OF THE INVENTION

5 This invention relates to crystalline ibuprofen having improved physical properties over previously known crystalline ibuprofen materials. More particularly, this invention provides an improved process for preparing crystalline ibuprofen of larger average particle length and improved flow properties.

BACKGROUND OF THE INVENTION

10 It is well known that alpha-arylalkanoic acids represent a large class of compounds, many of which are useful as anti-inflammatory and analgesic drugs.

 Among these, 2-(4-isobutylphenyl)-propionic acid known as Ibuprofen, 2-(3-phenoxyphenyl)-propionic acid known as Fenoprofen, 2-(2-fluoro-4-diphenyl)-propionic acid known as Flurbiprofen, 2-[4-(2-thienylcarbonyl)-phenyl]-propionic acid
15 known as Suprofen, 2-(6-methoxy-2-naphthyl)-propionic acid, whose S(+) isomer is known as Naproxen, and still others may be mentioned.

 The preparation of α -aryl propionic acids has so far followed the so-called classic chemical methods which employ as starting material aryl alkyl ketone derivatives and are known by such names as Darzen's reaction, Willgerodt's reaction,
20 Arndt-Eistert's reaction and Friedel-Crafts reaction. Of these, Darzen's reaction constitutes more or less the generally accepted basic method for the preparation of α -aryl propionic acids. [D.R. White (The Upjohn Company) U.S. Pat. No. 3,975,431 (1976); Chemical Abstracts 86,5168 w].

 More recently, newer methods have been proposed for the preparation of
25 α -aryl propionic acids. These include Gassman's procedure and certain nucleophilic substitution and chemical rearrangement of propionic acid derivatives [P.G. Gassman and T. J. Van Bergen, Journal of the American Chemical Society, 96(17), 5508 (1974); G. P. Stahly, B. C. Stahly and K. C. Lilge, Journal of Organic Chemistry, 49

579 (1984); M. S. Newman and B. J. Magertein, Organic Reactants V, 413 (1949); Brown, E. V. Synthesis, 358 (1975); S. Yoshimura, S. Takahashi and M. Ichino (Kohjin Company), Japanese Pat. No. 76/36432 (Mar. 27, 1976); and Chemical Abstract 85,123596 m].

5 While any of these preparation schemes produce the desired aryl propionic acid, very little attention has been paid to the methods of processing the materials produced. Thus, one of the highest commercial volume profen drugs, ibuprofen, is typically produced in a crystalline form that flows poorly. (It should be noted that
10 ibuprofen crystalline flow is directly related to total surface area and, therefore, crystal size, i.e., large crystals, promotes flow because of decreased surface area.) As a result, preparations containing this material disadvantageously adhere to the molding surfaces of tablet punches and dies during processing.

 In U. S. Patent No. 4,476,248, the course of the above disadvantageous behavior was established as due to the size and the shape of the ibuprofen crystals.
15 This patent discloses that acicular (needle) or lath (blade) crystals are to be avoided and cubic or spherical shapes are desirable. These latter shapes produce greatly enhanced crystalline flow properties of the final ibuprofen. The patent further discloses that when ibuprofen is dissolved in and crystallized from a solution of any solvent which has a hydrogen bonding parameter (SH) equal or greater than (\geq) 8
20 Hilderbrand units, e.g., a C₁ to C₃ alkanol, there is obtained crystalline ibuprofen having larger particle size, on average, as compared to crystalline ibuprofen obtained by crystallizing ibuprofen from heptane or hexane, the usual commercially used solvents.

 While this patent extols the economic advantages of such improved flow
25 produced from the larger particle size crystalline ibuprofen, the extra processing step, i.e., the step required to first remove the inert solvent (typically a hydrocarbon one) used in the above-disclosed processes for preparing the α -aryl propionic acid, is undesirably costly and time and equipment consuming.

 Accordingly, there is a need for preparing crystalline ibuprofen that has
30 improved flow properties over that of the prior art.

OBJECTS OF THE INVENTION

It is an object of this invention to produce an im-proved crystalline habit and crystal shape of ibuprofen, and to provide a process for preparing crystalline ibuprofen which has larger average particle length and improved flow properties compared to previously known bulk ibuprofen materials.

It is a further object of this invention to provide a crystalline ibuprofen which has larger average particle size range, having excellent flow properties, and the majority of said particles being rod-shaped crystals.

Other objects, aspects and advantages of this invention will become apparent from reading the remaining specification and the claims which follow.

SUMMARY OF THE INVENTION

Briefly, it has been found that when ibuprofen is dissolved in and crystallized from a saturated solution of a liquid hydrocarbon solvent in a specific procedure, there is obtained crystalline ibuprofen having larger particle length, on average, as compared to crystalline ibuprofen obtained by crystallizing ibuprofen from heptane or hexane as carried out by the conventional forms of commercial processing.

The crystalline ibuprofen obtained by the process of the present invention is recovered without the necessity of first removing the inert solvent disclosed in the prior art to provide crystalline ibuprofen. Such crystalline ibuprofen is subject to further recrystallization and purification utilizing a different solvent.

As a result of the process of the invention, a more cost effective manufacturing process can be developed by reducing pharmaceutical production down time, due to compressing problems (sticking and lamination), requiring less formulation time and handling, and eliminating energy cost required in the drying operations.

Thus, using the process of this invention in the crystallization of ibuprofen has improved its physical properties and the manufacturability of ibuprofen.

PHOTOMICROGRAPHS

Figures 1, 2, 3 and 4 are microscopic photographic exhibits of ibuprofen

crystals prepared by the process of the present invention.

Figure 5 is a microscopic photographic exhibit of ibuprofen crystals prepared by the process of the prior art.

DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

5 According to the process of the present invention, crystalline ibuprofen has been prepared having a crystalline habit characterized by having a particle length larger than about 75 microns average and a length to width aspect ratio of greater than about 4 to 1 to about 5 to 1. Preferably the particle length is from about 100-200 microns, most preferably from about 125 to about 175 microns. Preferred length
10 to width ratios are from about 4.1 to 1 to about 5 to 1.

 In the ibuprofen manufacturing processes, ibuprofen is crystallized from its reaction mixtures by precipitating it from an aqueous solution of the sodium ibuprofen salt, for example, by addition to that salt solution of an inorganic acid or from aqueous/heptane or aqueous/methylene chloride mixture, as known in the art.
15 The ibuprofen crystals produced in this way have a crystal aspect ratio averaging greater than 6. In contrast, according to this invention, we have discovered how to obtain ibuprofen crystals having a crystal aspect ratio averaging no greater than about 5 and as low as 4, for example, (after ibuprofen has been manufactured as above) by dissolving ibuprofen in the defined solvent media used in the process of this
20 invention without any substantial salt formation, and crystal-lizing the ibuprofen therefrom as described herein to obtain significantly improved crystal habit ibuprofen.

 Examples of liquid solvents for ibuprofen which will give the desired low aspect ratio ibuprofen crystal habit include the hydrocarbon solvents which include
25 the linear and branched hydrocarbons having the general formula $C_n H_{2n+2}$, where n is from 5 to 10, preferably from 6 to 8, most preferably 6 or 7. Particularly preferred is hexane. Mixtures of these hydrocarbon solvents may also be used in the process of this invention.

 The crystalline ibuprofen having the above-mentioned improved physical
30 properties can be prepared by crystallizing or precipitating the ibuprofen from one

or more of the above sol-vents by a number of methods. A preferred method can be described by the following sequence of steps:

(a) forming a saturated solution of ibuprofen in one or more of the liquid hydrocarbon solvents disclosed herein at a temperature of from about 20° C to about 5 60° C;

(b) seeding the saturated solution with solid ibuprofen;

(c) cooling the saturated and seeded solution to a temperature of about 0° to about -20° C at a rate to retard primary nucleation and promote secondary nucleation, thereby obtaining a slurry; and

10 (d) separating crystalline ibuprofen from the liquid phase of the slurry.

In carrying out the process of the present invention, it is important to first form a fully ibuprofen-saturated solution in the liquid hydrocarbon solvent. At 20° C, the amount of ibuprofen that forms a fully saturated solution using, for example, the liquid hydrocarbon hexane, is 7.3 grams/100 grams of solvent. At 60° C, 245 grams 15 of ibuprofen fully saturate 100 grams of hexane.

To the fully saturated solution of ibuprofen is then added seed crystals of ibuprofen. The crystal habit of the seed crystals is not important in controlling the formation of the final large, rod-like crystals of the present process. Thus, seed crystals obtained from crystallization of ibuprofen from cooled supersaturated 20 solutions (typically of the acicular or lath shape) and smaller than 20 microns may be used. Equally successful are crystals obtained by crushing the product produced from the cooled supersaturated solutions. Significantly, it has been discovered that primary nucleation of the seeded solution saturated with ibuprofen can be avoided during the cool down sequence if no more than 1.0 % by weight of solid ibuprofen 25 based on weight of saturated solution is added, but at least 0.01 % by weight of solid ibuprofen based on total weight of saturated solution. Preferably, about 0.015 % by weight to about 0.5 % by weight of seed crystals is added, most preferably about 0.02 % by weight to about 0.04 % by weight. Primary nucleation is defined as spontaneous and/or self-seeding types of nucleation. Secondary nucleation occurs 30 when crystal growth is induced by addition of crystal nuclei, e.g., ibuprofen crystallites.

While the fully saturated and seeded solution of ibuprofen can be cooled down to about 0°C to about -20°C in one continuous step over a period of up to 6 hours, it has been found advantageous to conduct such cooling to such lower temperatures in specific time/temperature intervals. Thus, a first cooling interval
5 requires the temperatures to be lowered by about 5 percent and held for about 10 minutes to about 180 minutes, preferably about 20 minutes to about 120 minutes, most preferably about 45 minutes to about 75 minutes. By this sequential lowering, a second and third temperature reduction by a similar amount and for about the same time is necessary before the last, and greatest, temperature reduction to about
10 0°C to about -20°C. Such cooling is preferentially carried out under conditions of agitation (stirring, rocking, etc.).

Separation of the slurry produced from the sequential cooling can be accomplished by any conventional method, i.e., filtration, centrifugation, etc.

The invention is further exemplified by the following detailed examples, which
15 are not intended as limiting the scope of the process of this invention.

EXAMPLES

Comparative

A commercial batch of ibuprofen was prepared from 43% solution of ibuprofen in hexane. The solution was cooled to 40°C and seeded with ibuprofen.
20 The mixture was cooled at 5°C/hour to 30°C and then cooled at 10°C/hour to -10°C. The slurry was centrifuged and the crystals were washed with cold hexane and vacuum dried in a ribbon dryer. The ibuprofen had poor flow characteristics with a strong lumping tendency. The photomicrograph of the crystals showed an average crystal length of 59 microns and an average width of 16 microns, with an average
25 aspect (l/w) of 3.7. (Figure 5)

Example 1

To 309 g of a 43% solution of crude ibuprofen in hexane 0.02 g of seed (smaller crystals of ibuprofen from hexane crystallization) was added at 42°C. The temperature was dropped to 40°C and held for one hour; the temperature was

dropped to 38°C and held for one hour; and the temperature was dropped to 36°C and held for one hour. The resultant mixture was then cooled to -10°C in 180 minutes. The crystals were filtered, washed with cold hexane and dried. The crystals were free flowing with little lumping tendency observed.

- 5 Photomicrographs of the crystals were taken 100 X and the crystal dimensions were measured. The average crystal length was 161 microns, the average width was 38, with an aspect ratio (L/W) of 4.2. (Figure 2)

Example 2

- 10 To 283 g of a 43% solution of ibuprofen in hexane 0.02 g of seed (smaller crystals of ibuprofen from hexane crystallization) was added at 42°C. The temperature was dropped to 40°C and held for 30 minutes and then the temperature was dropped to 36°C and held for one hour. The resultant mixture was then cooled to -10°C in three hours. The crystals were filtered, washed with cold hexane and dried. The crystals were free flowing with little lumping tendency observed.

- 15 Photomicrographs of the crystals were taken at 100 X and the crystal dimensions were measured. The average crystal length was 181 microns, the average width was 39, with an aspect ratio (L/W) of 4.6. (Figure 3)

Example 3

- 20 A solution of 128 g of ibuprofen in 170 g of commercial hexane was cooled from 50°C to 42°C and seeded with 0.02 g of ibuprofen. The temperature was lowered to 40°C and held for 30 minutes. The temperature was then lowered to 38°C and held for 30 minutes, and then lowered to 36°C and held for 30 minutes. The slurry was cooled to -6°C over 3-hour period. The slurry was suction filtered and the crystals were washed with cold hexane and air dried. The ibuprofen was free
25 flowing with little lumping tendency. The photomicrograph of the crystals show an average crystal length of 148 microns and an average width of 29 microns, with an average aspect (l/w) of 5.1. (Figure 4)

We claim:

1. A process for preparing crystalline ibuprofen having a crystal habit characterized by having a particle length larger than 150 microns average and a length to width aspect ratio of from about 4 to 1 to about 5 to 1 comprising

5 (a) forming a saturated solution of ibuprofen in a liquid hydrocarbon solvent at a temperature from about 20°C to about 60°C;

(b) seeding said saturated solution with solid ibuprofen;

(c) cooling said saturated solution to a temperature of about 0°C to about -20°C at a rate to retard primary nucleation and promote secondary nucleation to obtain a slurry; and

10 (d) separating the crystalline ibuprofen from the liquid phase of the slurry.

2. The process according to Claim 1 wherein said liquid hydrocarbon is selected from the group consisting essentially of pentane, hexane, heptane, octane and mixtures thereof.

3. The process according to Claim 2 wherein said liquid hydrocarbon is hexane, heptane or mixtures thereof.

4. The process according to Claim 3 wherein said liquid hydrocarbon is hexane.

5. The process according to Claim 1 wherein said temperature of said saturated solution is about 30°C to about 50°C.

6. The process according to Claim 5 wherein said temperature is about 40°C to about 45°C.

7. The process according to Claim 1 wherein the amount of said seeding is about 0.01% to about 1.0% by weight of solid ibuprofen based on the total weight of solution.

8. The process according to Claim 7 wherein the amount of said seeding is about 0.015% to about 0.5% by weight.

9. The process according to Claim 8 wherein the amount of said seeding is about 0.02% to about 0.04% by weight.

10. The process according to Claim 1 wherein said cooling is carried out at four sequentially lower temperatures.

11. The process according to Claim 11 wherein said time interval is from about 20 minutes to about 120 minutes.

12. The process according to Claim 12 wherein said time interval is from about 45 minutes to about 75 minutes.

13. The process according to Claim 1 wherein said saturated solution with solid ibuprofen is agitated.

14. Crystalline ibuprofen having a crystal habit characterized by having a particle length larger than 75 microns average and a length to width aspect ratio of greater than 4 to 1.

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FIGURE 1.



FIGURE 2.

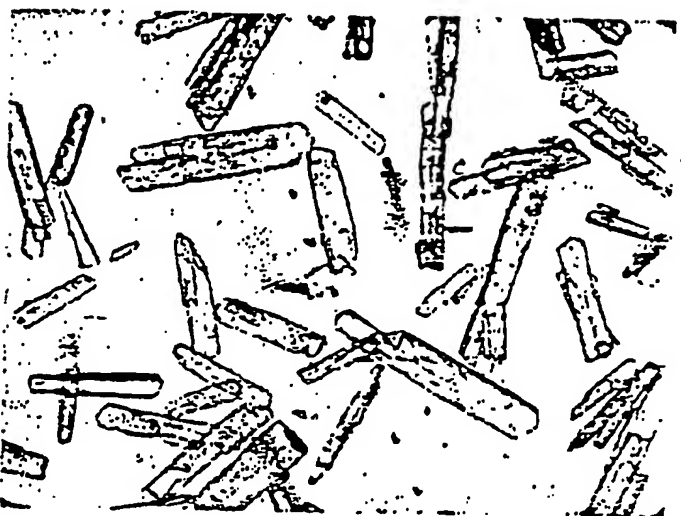


FIGURE 3.



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FIGURE 4.

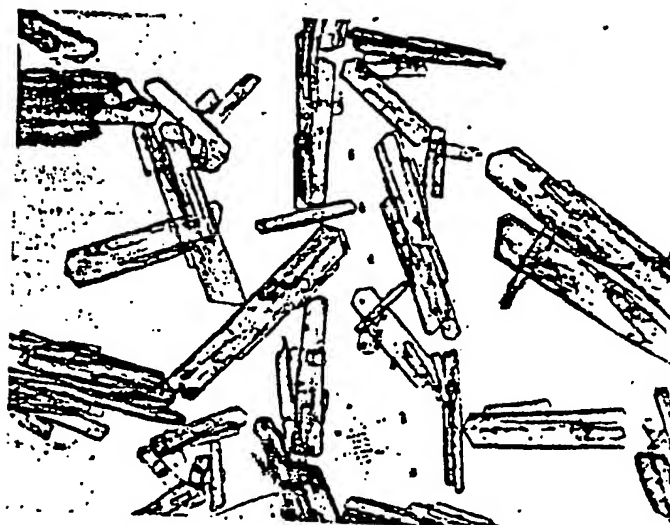


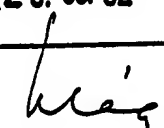
FIGURE 5.



INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 91/07991

I. CLASSIFICATION OF SUBJECT MATTER (If several classification symbols apply, indicate all) ⁶		
According to International Patent Classification (IPC) or to both National Classification and IPC Int.Cl. 5 C07C51/43		
II. FIELDS SEARCHED		
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III. DOCUMENTS CONSIDERED TO BE RELEVANT⁹		
Category ¹⁰	Citation of Document, ¹¹ with indication, where appropriate, of the relevant passages ¹²	Relevant to Claim No. ¹³
,,Y	EP,A,0 120 587 (THE UPJOHN COMPANY) 3 October 1984 cited in the application see claims 4,5,9,10 ---	1
Y	EP,A,0 170 147 (NIPPON PETROCHEMICALS COMPANY) 5 February 1986 see page 23, line 11 - line 12 see page 45, line 12 - line 14 see page 46, line 20 - line 22 ---	1
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IV. CERTIFICATION		
Date of the Actual Completion of the International Search 12 MARCH 1992	Date of Mailing of this International Search Report 20. 03. 92	
International Searching Authority EUROPEAN PATENT OFFICE	Signature of Authorized Officer KLÁG M. J. 	

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EP-A-0120587	03-10-84	US-A- 4476248	09-10-84
		AU-B- 567125	12-11-87
		AU-A- 2377184	06-09-84
		CA-A- 1212693	14-10-86
		JP-A- 59167536	21-09-84
EP-A-0170147	05-02-86	JP-A- 61024534	03-02-86
		JP-A- 61024537	03-02-86
		US-A- 4694100	15-09-87

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